Commonwealth of Kentucky Division for Air Quality

PERMIT APPLICATION SUMMARY FORM

Completed by: Ralph Gosney, P.E.

Gene	<u>ERAL INFORMATION:</u>		
	Name:	Free Flow Packaging International, Inc.	
	Address:	1 Graham Way	
		Hopkinsville, Kentucky	
	Date application received:	November 10, 2003	
	SIC/Source description:	3086/ Foamed polyethylene sheets manufacturing source	
	Source I. D. No.:	21-047-00099	
	Source AI No.:	37673	
	Activity No.:	APE20040001	
	Permit number:	V-05-068	
APPL	ICATION TYPE/PERMIT ACTIVIT	ΓY:	
	[] Initial issuance		
	Permit modification	[] Conditional major	
	Administrative	[X] Title V	
	— Minor	[] Synthetic minor	
	Significant	[X] Operating	
	[X] Permit renewal	[]Construction/operating	
Сом	DI LANCE CHAMADAY		
COMI	PLIANCE SUMMARY:	naa [] Complianaa sahadula inaludad	
	[] Source is out of complia [X] Compliance certification		
	[11] Compitance certification		
APPL	ICABLE REQUIREMENTS LIST:		
	[] NSR	[] NSPS [X] SIP	
	[]PSD	[] NESHAPS [] Other	
	[] Netted out of PSD/NSR		
		1(23)(b) or 51:052,1(14)(b)	
Misc	ELLANEOUS:		
	Acid rain source		
	[] Source subject to 112(r)		
		ally enforceable emissions cap	
		or alternative operating scenarios	
	[] Source subject to a MAC	<u>. </u>	
		y-case 112(g) or (j) determination	
	[] Application proposes ne	•	
	[X] Certified by responsible		
	[] Diagrams or drawings included		
	[] Confidential business information (CBI) submitted in application		
	[] Pollution Prevention Me	* * * * * * * * * * * * * * * * * * *	
	[] Area is non-attainment (list pollutants)	
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EMISSIONS SUMMARY (1):

Pollutant	Potential (tpy)	Actual (tpy) ⁽²⁾
PM/PM10	0.17	0.00
SO_2	0.17	0.00
NOx	2.25	0.00
VOC	370.71	125.84
СО	0.54	0.00
Hexane (HAP)	0.04	0.00
Total HAPs	0.04	0.00

Notes:

- (1) Please refer Appendix A of the Statement of Basis for detailed emission calculations (Pages 1 through 5).
- (2) Actual emissions are based on Emissions Inventory System report for 2005.

Source Process Description:

Free Flow Packaging International (F P International), Incorporated produces foamed polyethylene and polystyrene sheets for packaging. In the polyethylene foam plant, polyethylene along with isobutane, ethane, and glycerol monostearate are used as the raw materials and are injected into the extruder. The extruded foamed polyethylene sheets go through the slit tube and winder. The wound foamed polyethylene sheets are stored in the warehouse. The bad sheets (approximately 8%) are reprocessed to get polyethylene resin. The major emissions from this process are the VOC's (Isobutane emissions). The source also has isobutane and ethane storage tanks. The isobutane tanks are pressurized tanks. The ethane tanks are tube trailers and are not filled on site. They are replaced as needed.

In the polystyrene loosefill plant, polystyrene is fed to an extruder where it is melted and pressurized and injected with a blowing agent mixture of isopentane and isobutane. As the material exits the extruder it creates a plastic foam which is then formed into a trademark "Figure 8" cross-section, cooled, and cut into finite pieces. The cut particles from the extrusion line are then passed through an expander where they are exposed to live steam. The particles are then held for several hours in the intermediate storage silos while additional expansion occurs. The particles are then put through a second expansion step in which they are again exposed to live steam. The expanded product is dried in the hot room, which is heated to approximately 140°F. The product from the hot room is transferred to the warehouse where it is stored until it is packaged in fourteen cubic foot bags or loaded directly into bulk trailers for shipment.

The source consists of the following permitted emission units:

- (a) Polyethylene (PE) Foam Plant, consisting of:
 - (1) One (1) foam extrusion line, consisting of polyethylene foam sheet extruder, slit tube and winder, identified as P-1 and constructed in June 1999, with a maximum foam sheet processing rate of 419 tons per year, and exhausting to one (1) stack P1;
 - (2) One (1) PE scrap reprocessing operation, identified as P-2 and constructed in June

- 1999, with a maximum foam sheet processing rate of 419 tons per year, and exhausting to one (1) stack P2;
- (3) One (1) PE foam sheet warehouse, identified as W-1 and constructed in June 1999, with a maximum foam sheet processing rate of 419 tons per year, and exhausting inside the building.
- (b) Polystyrene (PS) Loosefill Plant, consisting of:
 - (1) One (1) PS extrusion line, consisting of polystyrene loosefill extruder, identified as P-3 and constructed in 2001, with a maximum foam processing rate of 148 tons per year, and exhausting to one (1) stack P3;
 - One (1) PS expansion equipment, identified as P-4 and constructed in 2001, with a maximum foam processing rate of 148 tons per year, and exhausting to one (1) stack P4;
 - (3) PS intermediate storage and hot room, identified as W-2 and constructed in 2001, with a maximum foam processing rate of 148 tons per year, and exhausting inside the warehouse;
 - (4) PS product storage, identified as W-3 and constructed in 2001, with a maximum processing rate of 148 tons per year, and exhausting inside the warehouse;
- (c) One (1) natural gas fired boiler, identified as B-1, constructed in 2005, with a maximum heat input rate of 5.23 million British thermal units per hour, exhausting through one (1) stack B1; and
- (d) One (1) crystal clean cold cleaning degreaser, identified as EP-1, with a maximum solvent consumption rate of 24 gallons per year.

Emission and Operating Caps Description:

The source requested to limit VOC emissions from the PE foam plant and PS loosefill plant to less than 245 tons per year and 225 tons per year, respectively. The source is not restricted as to hours of operation or quantity of product produced while remaining within these emissions limitations.